

# LATTICE-BOLTZMANN SCHEME FOR DENDRITIC GROWTH IN PRESENCE OF CONVECTION

Dmitry Medvedev, Klaus Kassner

Institute of Theoretical Physics, Otto-von-Guericke-University, Universitätsplatz 2, 39106 Magdeburg, Germany e-mail: dmedv@physik.uni-magdeburg.de

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# **SUMMARY**

A combined phase-field/lattice-Boltzmann scheme is proposed to simulate dendritic growth from supercooled melt, with account for flows of liquid and thermal convection.

# MODEL

- 1. Simulation of solidification phase-field model (Karma and Rappel, 1996).
- 2. Flow of liquid lattice-Boltzmann-BGK (LBGK) method with incorporated interactions with solid and thermal convection. This step can be left out in the case of purely diffusional growth.
- 3. Conductive and convective heat transfer multicomponent LBGK method.

### Phase-field model

$$
\tau(\theta)\phi_t = (2\phi - 1 - 4\lambda \overline{T}\phi(1-\phi))2\phi(1-\phi) + \nabla \cdot (W^2(\theta)\nabla \phi) - \partial_x (W(\theta)W'(\theta)\phi_y)) + \nabla \cdot (\overline{W^2}(\theta)\nabla \phi) - \partial_y (W(\theta)W'(\theta)\phi_x),
$$
\n
$$
\overline{T}_t + \mathbf{U}\nabla \overline{T} = D\nabla^2 \overline{T} + \phi_t.
$$

 $\phi$  — concentration of solid phase  $(0 \le \phi \le 1)$ ,  $\overline{T} = \rho c_p (T - T_m)/L$  — normalized temperature,  $W$  — anisotropic interface width,  $\tau$  — relaxation time.

In order to obtain zero kinetic coefficient, the following relations must be imposed

$$
W = W_0 A(\theta), \ \tau = \tau_0 A^2(\theta), \ \lambda = \frac{2ID\tau_0}{(K + JF)W_0^2}.
$$

Anisotropy function

$$
A(\theta) = 1 + \varepsilon \cos 4\theta,
$$

 $\theta = \arctan(\phi_y/\phi_x)$  — the angle between the local interface normal and the X axis. We assume  $\tau_0 = 1$ ,  $W_0 = 1$ . Interface stiffness  $\alpha = 15\varepsilon$ .

This equation was discretized on a uniform spatial lattice with a step  $\Delta x = 0.4$ , and solved using the explicit Euler method with time step  $\Delta t$ .

## Lattice-Boltzmann method

- Regular lattice, lattice vectors  $\mathbf{e}_k$
- Discrete set of velocities  $\mathbf{c}_k \Delta t_{LB} = \mathbf{e}_k$

Variables  $f_k$  — one-particle distribution functions. Evolution equation

$$
f_k(t, \mathbf{x}) = f_k(t - \Delta t_{LB}, \mathbf{x} - \mathbf{c}_k \Delta t_{LB}) + \frac{f_k^{eq} - f_k}{\tau_f}.
$$

Propagation and collisions,  $\tau_f$  — Maxwellian relaxation time. Later on  $\Delta t_{LB} = 1$ . Kinematic viscosity  $\nu = (\tau_f - 1/2)/3$ . Hydrodynamic quantities

$$
\rho = \sum_{k} f_k, \qquad \rho \mathbf{U} = \sum_{k} f_k \mathbf{c}_k.
$$

Equilibrium distribution functions  $f_k^{eq}$  $k^{eq}(\rho, \mathbf{U}).$ Interaction with solid

$$
\mathbf{F}_d = -\nu \frac{2h\phi^2}{W_0^2} \mathbf{U}.
$$

Thermal convection — buoyancy force

$$
\mathbf{F}_c = -\rho \alpha (1-\phi) (\overline{T}-\overline{T}_0) \mathbf{g},
$$

 $\alpha$  — coefficient of thermal expansion,  $\mathbf{g}$  — gravity acceleration.

### Heat transport

Second set of distribution functions  $N_k$ . Evolution equation

 $N_k(t + \Delta t, \mathbf{x} + \mathbf{c}_k \Delta t) = N_k(t, \mathbf{x}) + \frac{N_k^{eq} - N_k}{t}$  $\tau_{T}$ .  $N_k^{eq} = N_k^{eq}$  $\chi^{eq}_k(\overline{T},{\bf U}+\Delta{\bf U}/2)$  $\overline{T}=\Sigma$ k  $N_k$ ,  $\mathbf{U} = \sum_{k=1}^{N_k}$ k  $f_k \mathbf{c}_k / \sum$ k  $f_k$ ,  $\Delta \mathbf{U} = \mathbf{F}/\sum$ k  $f_k$  $\mathbf{F} = \mathbf{F}_d + \mathbf{F}_c$  — total force. Resulting equation

$$
\frac{\partial \overline{T}}{\partial t} = \mathbf{U}\nabla \overline{T} + \chi \nabla^2 \overline{T} + \frac{\partial \phi}{\partial t}.
$$

Thermal diffusivity  $\chi = (\tau_T - 1/2)/3$  everywhere (symmetric model).

### Shear flow



Figure 1: Dendrite.  $\Delta = 0.7, 15\varepsilon = 0.15$ . Reduced velocity  $\overline{U}=0$  (a),  $\overline{U}=0.0123$ (b),  $\overline{U}=0.0247$  (c),  $\overline{U}=0.0493$  (d). Interface contours are shown at time increments of 50



Figure 2: Seaweed.  $\Delta = 0.8, 15\varepsilon = 0.15.$  Reduced velocity  $\overline{U}=0$  (a),  $\overline{U}=0.0247$ (b),  $\overline{U}=0.0493$  (c),  $\overline{U}=0.0987$  (d). Interface contours are shown at time increments of 20

### Thermal convection



Figure 3: Dendritic growth with convection.  $\Delta = 0.8, 15\varepsilon = 0.3$ .  $\beta g_y = 0.0$ ,  $g_x = 0$  (a);  $\beta g_y = -0.0005$ ,  $g_x = 0$  (b);  $\beta g_y = 0.0005$ ,  $g_x = 0$  (c) and  $g_y = 0$ ,  $\beta g_x = 0.0005$  (d). Interface contours are shown at time increments of 10

### Influence of parallel flow on the growth

Growth of the dendrite tip in the parallel flow

 $\Delta = 0.65, 15\varepsilon = 0.75$ , grid size 300×600



Figure 4: Dependence of reduced velocity  $\overline{V}$  and selection parameter  $\sigma$  on flow Reynolds number.  $1 - \overline{V}, \nu = 1/3; 2 - \sigma, \nu = 1/3; 3 - \overline{V}, \nu = 1/6; 4 - \sigma$  $\sigma, \nu = 1/6$ 



Figure 5: Dependence of reduced tip radius  $\bar{\rho}$  on reduced flow velocity  $\bar{U}$ 



Figure 6: Dependence of reduced velocity  $\overline{V}$  and selection parameter  $\sigma$  on reduced flow velocity  $\overline{U}$ 



Figure 7: Dependence of reduced tip radius  $\bar{\rho}$  on reduced flow velocity  $\bar{U}$ 

Dependences  $\overline{V} \sim \overline{U}^{0.38}$ ,  $\overline{R} \sim \overline{U}^{-0.16}$ ,  $\sigma \sim \overline{U}^{-0.04}$ 



Figure 8: Dependence of reduced velocity  $\overline{V}$  and selection parameter  $\sigma$  on flow Reynolds number



Figure 9: Dependence of reduced tip radius  $\bar{\rho}$  on reduced flow velocity  $\bar{U}$ 

# Growth of the dendrite tip in the parallel flow

#### Sidebranching in the parallel flow



Figure 10: Growth of side branches,  $\Delta = 0.7, 15\varepsilon = 0.15$ . Reduced flow velocity  $\overline{U} = 0.01$  (a) and  $\overline{U} = 0.04$  (b)

At large flow velocities, oscillations of tip velocity were observed, accompanied by the enhanced growth of side branches.

# **Conclusions**

The main results are

- Simulations showed strong influence of external shear flow on the seaweed growth (Fig. 2)
- Influence of parallel flow on the operation state of dendrite tip was investigated quantitatively (Fig. 4–9)
- Simulations demonstrated onset of velocity oscillations and enhancement of sidebranching under parallel flow (Fig. 10)